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# Progress in Developing an Open Burn/ Open Detonation Dispersion Model

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## INTRODUCTION

Obsolete or unwanted munitions, rocket propellants, and manufacturing wastes require treatment at Department of Defense (DOD) and Department of Energy (DOE) facilities. One of the most widely-used treatment methods is open burning (OB) and open detonation (OD) of the material. Currently, the material destroyed in a single detonation generally ranges from 100 to 5000 lbs, while the quantity removed by a burn can be larger and last from minutes to an hour. OB/OD operations are confined to daytime with atmospheric stability conditions ranging from convective or highly unstable to near neutral.

OB/OD activities produce air pollutants and require predictions of pollutant concentrations to obtain an operating permit. The pollutants include  $\text{SO}_2$ ,  $\text{NO}_x$ , particulates, volatile organic compounds and toxic materials such as metals, semivolatile organics, etc.<sup>1</sup> Large detonations also generate large quantities of dust/soil that are entrained by the rising contaminant cloud. OB/OD sources differ from most traditional air pollution sources in that they have: 1) instantaneous or short-duration releases of buoyant material rather than continuous releases, and 2) ambient exposure times for the clouds that can be much less than the typical averaging times ( $\geq 1$  hr) of air quality standards.

Atmospheric dispersion models are used to estimate pollutant concentrations given information on the source and meteorological conditions. However, there is currently no recommended EPA dispersion model to address the unique features of OB/OD sources. The most commonly-used approach is INPUFF,<sup>2</sup> a Gaussian puff model, but this has several limitations as briefly discussed below and elsewhere.<sup>3</sup> As a result, a model development program was initiated under the DOD/DOE Strategic Environmental Research and Development Program.

This paper briefly summarizes the model development effort which is divided into "operational" and "research" components. In the following, we give a brief discussion of the background and overall model design and then describe the operational model components for instantaneous (OD) and short-duration (OB) sources; the OD model is a Gaussian puff approach whereas the OB framework consists of integrated-puff and plume models. The combined OB/OD model includes: 1) a continuous treatment of dispersion as the release condition varies from instantaneous to continuous, 2) cloud and plume rise obtained from appropriate entrainment models, 3) cloud and plume penetration of elevated inversions, 4) relative (puff) and total dispersion based on modern scaling concepts for the planetary boundary layer (PBL), and 5) a capability for the use of onsite profiles of wind, temperature, and turbulence from a mobile meteorological platform. The current OB/OD model focuses on the unstable PBL.

## BACKGROUND AND MODEL DESIGN

### Background

The development of an OB/OD dispersion model has considered: 1) the limitations of existing models, 2) current knowledge of turbulence and dispersion in the PBL, and 3) a mobile meteorological platform under development.

**Limitations of existing models.** INPUFF has been used to model OB/OD sources and can handle dispersion from individual puffs or clouds or from a sequence of puffs in a short-duration release. Although the Gaussian puff approach is suitable for OB/OD sources, INPUFF has the following limitations: 1) It adopts dispersion parameters ( $\sigma_y, \sigma_z$ ) from the Pasquill-Gifford (PG) curves. 2) It includes Briggs' (Ref. 4) plume rise expressions which apply to continuous releases rather than to instantaneous sources (puffs, clouds) and does not address thermal penetration of elevated inversions capping the PBL. 3) It assumes Gaussian velocity statistics for the turbulence, whereas the vertical velocity statistics in the unstable PBL are positively skewed.<sup>5</sup> The skewness should be included for vertical dispersion.

For OB/OD sources, the PG curves are deficient in that they: 1) are based on dispersion from a ground-level source and short downwind distances ( $< 1$  km), and 2) are selected using surface meteorology, which does not account for the PBL's vertical structure. For large detonations, source buoyancy can carry emissions to several 100 m or the PBL top; one must then deal with dispersion over the entire PBL.

**PBL turbulence.** Dispersion in the PBL depends on the turbulence length and velocity scales which differ for the unstable or convective boundary layer (CBL) and the stable boundary layer (SBL). For the CBL, the length and velocity scales are the CBL depth  $h$  and the convective velocity scale  $w_*$ ;  $w_* = (g\overline{w\theta}_o h / \Theta_a)^{1/3}$ , where  $g$  is the gravitational acceleration,  $\overline{w\theta}_o$  is the turbulent heat flux at the surface, and  $\Theta_a$  is the ambient potential temperature. Typical values of  $w_*$  and  $h$  at midday over land are 1 - 2 m/s and 1 - 2 km. Within the "mixed layer" ( $0.1h \leq z < h$ ), the mean wind speed and turbulence components—longitudinal  $\sigma_u$ , lateral  $\sigma_v$ , and vertical  $\sigma_w$ —vary little with height  $z$ ; in strong convection,  $\sigma_u, \sigma_v, \sigma_w \simeq 0.6w_*$ .

For the SBL, the turbulence is much weaker with eddy sizes proportional to  $z$  near the surface and typically  $\sim 10$ s of meters or less in the upper part of the SBL. Models and observations show that the velocity scale is the friction velocity  $u_*$  (Ref. 5), which is typically  $\sim 0.1$  m/s in strong stable stratification.

Knowledge of the PBL turbulence structure has been included in a number of models for air quality applications.<sup>6</sup> One example is AERMOD<sup>7</sup> for industrial source complexes.

**Mobile meteorological platform.** A mobile meteorological platform is being developed at NOAA's Environmental Technology Laboratory to obtain the PBL variables necessary for modeling since many DOD facilities are in remote locations. The platform design includes: 1) a radar wind profiler for obtaining the three wind

components up to  $\sim 3$  km. 2) a radio acoustic sounding system (RASS) for temperature measurements. 3) a mini-SODAR for measuring winds and  $\sigma_w$  to a height of  $\sim 200$  m. 4) a mini-lidar system for obtaining the PBL depth  $h$ , and 5) a portable meteorological station for measuring near-surface winds, temperature, turbulence, and heat flux. The dispersion model is being designed for efficient use of these measurements.

### Overall Model Design

The overall model design includes: 1) a simple computational or operational framework for routine problems, and 2) a more detailed or research model for nonroutine problems. In the operational approach, a Gaussian puff model is adopted for instantaneous sources and puff, integrated-puff, and plume models for short-duration releases. For the research framework, a Lagrangian particle and/or puff approach is planned. Both frameworks will be considered for "onsite" use in a real-time operational mode using data from the mobile meteorological platform, i.e., for day-to-day decisions on OB/OD operations. The operational puff and plume models would be used for climatological analyses needed in risk assessments.

In modeling, the important aspects to address are: 1) all source-related features including the instantaneous or short-duration nature of the release, buoyancy-induced rise and dispersion, and cloud or plume penetration of elevated inversions, 2) relative and absolute dispersion expressions that explicitly include PBL turbulence variables, 3) meteorological variables including their vertical profiles from the mobile platform, and 4) a treatment for puff and plume dispersion about complex terrain.

The models discussed in the following sections address points 1 and 2 above and must be expanded to include points 3 and 4. Further development also will address: 1) a more complete description of initial source effects (detonation cloud size and height) and inversion penetration, 2) a more complete PBL turbulence parameterization, 3) averaging time effects on concentration, 4) the entrained dust source term, and 5) deposition of gases and particles.

## INSTANTANEOUS SOURCES

### Dispersion Model

In many OB/OD applications, estimates of peak ground-level concentrations (GLCs) are required for averaging times ranging from seconds or minutes to an hour or longer. In making such estimates, we must account for the stochastic or random nature of turbulence and dispersion in the PBL. That is, we must recognize that the observed concentration at a receptor is a random variable and should be predicted statistically through a probability distribution.<sup>8,9</sup> The distribution can be parameterized by a functional form such as a gamma or clipped-normal distribution<sup>9</sup> and requires a minimum of two variables to characterize it—the mean concentration  $C$  and the root-mean-square (rms) concentration fluctuation  $\sigma_c$ , which is a measure of the width of the distribution. The peak concentration then can be defined by a specified percentile value of the cumulative probability distribution, e.g., the 99.9th percentile level. In the

following, we discuss approaches for predicting  $C$ ,  $\sigma_c$ , cloud rise, and the dispersion parameters: the functional form of the distribution remains to be selected.

**Mean concentration.** For instantaneous sources or detonations, a Gaussian puff model is adopted for predicting the short-term mean concentration ( $C$ ) field relative to the puff centroid. The  $C$  is the expected or average concentration that would be observed if the same experiment—same source and meteorological conditions—were repeated a large number of times.<sup>9</sup> The  $C$  is given by:

$$C = \frac{Q}{(2\pi)^{3/2}\sigma_{rx}\sigma_{ry}\sigma_{rz}} \exp \left[ -\frac{(x - Ut)^2}{2\sigma_{rx}^2} - \frac{y^2}{2\sigma_{ry}^2} - \frac{(z - h_e)^2}{2\sigma_{rz}^2} \right], \quad (1)$$

where  $Q$  is the pollutant mass released,  $U$  is the mean wind speed,  $t$  is the travel time,  $h_e$  is the effective puff height, and  $\sigma_{rx}$ ,  $\sigma_{ry}$ , and  $\sigma_{rz}$  are the puff standard deviations or relative dispersion parameters in the  $x$ ,  $y$ , and  $z$  directions, respectively. Here,  $h_e = h_s + \Delta h(x)$  where  $h_s$  is the source height which is generally zero for OB/OD sources, and  $\Delta h$  is the cloud rise due to buoyancy;  $x$  and  $y$  are the distances in the mean wind and crosswind directions.

The maximum mean concentration  $C_c$  at the puff centroid is given by  $C_c = Q/[(2\pi)^{3/2}\sigma_{rx}\sigma_{ry}\sigma_{rz}]$ , where the relative dispersion parameters are generally different in the three directions. In the following, we assume  $\sigma_{rx} = \sigma_{ry} = \sigma_{rz} = \sigma_r$ .

The  $C$  field including puff meandering is given by Eq. (1), but with  $\sigma_{rx}, \sigma_{ry}, \sigma_{rz}$  replaced by the absolute dispersion parameters— $\sigma_x, \sigma_y, \sigma_z$ . A Gaussian distribution for  $C$  is applicable in the SBL where the probability density function (p.d.f.),  $p_w$ , of the vertical velocity  $w$  is Gaussian. However, for the CBL, a skewed  $w$  p.d.f. is more consistent with laboratory and field data. A skewed p.d.f. is adopted here and is parameterized by the superposition of two Gaussian distributions.<sup>10</sup>

The  $C$  field due to an ensemble of meandering puffs is derived from  $p_w$  following the same approach as applied to continuous plumes.<sup>10</sup> The resulting expression for  $C$  is

$$C = \frac{Q}{(2\pi)^{3/2}\sigma_x\sigma_y} \exp \left( -\frac{(x - Ut)^2}{2\sigma_x^2} - \frac{y^2}{2\sigma_y^2} \right) \times \sum_{j=1}^2 \frac{\lambda_j}{\sigma_{zj}} \exp \left( -\frac{(z - h_e - \bar{z}_j)^2}{2\sigma_{zj}^2} \right), \quad (2)$$

where  $\sigma_{zj} = \sigma_{wj}x/U$  and  $\bar{z}_j = \bar{w}_j x/U$  with  $j = 1, 2$ . The  $\lambda_j$ ,  $\bar{w}_j$ , and  $\sigma_{wj}$  ( $j = 1, 2$ ) are the weight, mean velocity, and standard deviation of each Gaussian p.d.f. comprising  $p_w$ . Equation (2) applies for short distances such that the plume interaction with the ground or elevated inversion is weak. The complete expression for  $C$  includes multiple cloud reflections at the ground and PBL top.

The time-averaged concentration can be found from the dose where the partial dose is defined by  $\psi(x, y, z, t) = \int_0^t C(x, y, z, t') dt'$  and the total dose by  $\psi_\infty = \psi(x, y, z, \infty)$ . For clouds with short passage times over a receptor, the average concentration  $\bar{C}$  can be obtained from  $\bar{C} = (\psi(t_2) - \psi(t_1))/T_a$ , where the averaging time  $T_a = t_2 - t_1$ . If the puff passage time  $4\sigma_{rx}/U$  is less than  $T_a$ , then  $\bar{C} = \psi_\infty/T_a$ .

**Rms concentration fluctuation.** For elevated sources such as a buoyant cloud, the rms concentration fluctuation at the ground is largest close to the source and decreases with increasing distance.<sup>9,11</sup> As a first step in predicting  $\sigma_c$ , we adopt Gifford's<sup>12</sup> meandering plume or cloud model which applies to the near-source region; specifically, it applies when the large-scale eddies in the PBL cause the wandering or meandering of a small growing plume or cloud. The cloud only occasionally reaches the ground, but it does so in high concentration due to the small local spread  $\sigma_r$ ; thus, it creates large "spikes" in the GLC distribution and a large concentration variance.<sup>11</sup> In the following, we model the mean square concentration  $\langle c^2 \rangle$ , where the angle brackets denote an ensemble average, and then find  $\sigma_c$  from  $\sigma_c = (\langle c^2 \rangle - C^2)^{1/2}$  (see Ref. 9).

In Gifford's model, the instantaneous concentration distribution in a cloud is assumed to be a nonrandom, axisymmetric Gaussian distribution about the instantaneous cloud centroid  $\mathbf{x}_c = (x_c, y_c, z_c)$ :

$$c(\mathbf{x}, \mathbf{x}_c) = \frac{Q}{(2\pi)^{3/2} \sigma_r^3} \exp \left[ -\frac{(x - x_c)^2}{2\sigma_r^2} - \frac{(y - y_c)^2}{2\sigma_r^2} - \frac{(z - z_c)^2}{2\sigma_r^2} \right]. \quad (3)$$

Concentration fluctuations arise due to the randomness in  $x_c, y_c$  and  $z_c$ , which is caused by the meandering of the cloud.

The  $\langle c^2 \rangle$  is obtained by averaging the quantity  $c^2$  from Eq. (3) over the joint displacement p.d.f.,  $p(\mathbf{x}_c, t)$ , which is a function of time. In the well-mixed CBL, the turbulent velocity fluctuations in the  $x, y, z$  directions are uncorrelated throughout the bulk of the layer; likewise, the centroid displacements in the three directions should be uncorrelated random variables. Thus, assuming independence of the displacements in the three directions, we have  $p(\mathbf{x}_c, t) = p_x(x_c, t) \cdot p_y(y_c, t) \cdot p_z(z_c, t)$ . Using Gifford's approach, the  $\langle c^2 \rangle$  is found from

$$\langle c^2 \rangle = \int_{x_c} \int_{y_c} \int_{z_c} c^2(\mathbf{x}; \mathbf{x}_c) p_x(x_c, t) \cdot p_y(y_c, t) \cdot p_z(z_c, t) dx_c dy_c dz_c. \quad (4)$$

The displacement p.d.f.s in (4) are found from the velocity p.d.f.s— $p_u(u)$ ,  $p_v(v)$ , and  $p_w(w)$ , where  $u, v, w$  are the random velocity components in the  $x, y, z$  directions. Close to the source, we assume that  $x_c = ut$ ,  $y_c = vt$ , and  $z_c = h_e + wt$ . The  $p_x, p_y$  and  $p_z$  can then be derived as in Weil.<sup>10</sup> Taking  $p_u$  and  $p_v$  as Gaussian, one finds

$$p_x(x_c) = \frac{1}{\sqrt{2\pi}\sigma_x} \exp \left[ -\frac{(x_c - \langle x_c \rangle)^2}{2\sigma_x^2} \right], \quad p_y(y_c) = \frac{1}{\sqrt{2\pi}\sigma_y} \exp \left[ -\frac{y_c^2}{2\sigma_y^2} \right], \quad (5)$$

where  $\sigma_x = \sigma_u t$ ,  $\langle x_c \rangle = Ut$ , and  $\sigma_y = \sigma_v t$ . For  $p_w$ , a bi-Gaussian p.d.f. or superposition of two Gaussian distributions is adopted, which results in a similar distribution for  $p_z$  as noted earlier (Eq. 2).

By substituting the derived  $p_x, p_y$ , and  $p_z$  into Eq. (4) and carrying out the integration, we obtain

$$\langle c^2 \rangle = \frac{Q^2}{(2\pi)^3 \sigma_r^3 \sigma_{xe} \sigma_{ye}} \exp \left( -\frac{(x - Ut)^2}{\sigma_{xe}^2} - \frac{y^2}{\sigma_{ye}^2} \right) \times \sum_{j=1}^2 \frac{\lambda_j}{\sigma_{zej}} \exp \left( -\frac{(z - h_e - \bar{z}_j)^2}{\sigma_{zej}^2} \right), \quad (6)$$

where  $\sigma_{xe} = (\sigma_r^2 + 2\sigma_x^2)^{1/2}$ ,  $\sigma_{ye} = (\sigma_r^2 + 2\sigma_y^2)^{1/2}$ , and  $\sigma_{zej} = (\sigma_r^2 + 2\sigma_{zj}^2)^{1/2}$  with  $j = 1$  or  $2$ . The  $\lambda_j$ ,  $\bar{z}_j$ , and  $\sigma_{zj}$  are the same variables as in Eq. (2). The above  $\langle c^2 \rangle$  expression applies to short distances such that the cloud interaction with the ground and elevated inversion is weak; similar to Eq. (2), we include reflections at  $z = 0, h$  to obtain the complete expression for  $\langle c^2 \rangle$ .

Note that Eq. (6) is of the same form as Eq. (2) except for the omission of the 2 in the denominator of the exponential terms. This is consistent with the  $\langle c^2 \rangle$  expression for passive releases in Gaussian turbulence (see Refs. 11 and 12).

**Cloud rise and inversion penetration.** Scorer<sup>13</sup> combined theory and laboratory experiments to obtain the following expression for cloud rise in a neutral environment

$$\Delta h = 2.35(M_T t + F_T t^2)^{1/4} \quad (7)$$

$M_T$  and  $F_T$  are the initial momentum and buoyancy of the cloud and are given by

$$M_T = \frac{4\pi}{3} r_o^3 w_o \quad \text{and} \quad F_T = \frac{g Q_T}{c_p \rho_a \Theta_a} \quad (8)$$

where  $w_o$ ,  $r_o$ , and  $Q_T$  are the initial velocity, radius, and heat content of the thermal,  $c_p$  is the specific heat of air, and  $\rho_a$  and  $\Theta_a$  are the ambient air density and potential temperature. The  $Q_T$  can be determined from the mass of the detonation and its heat content,  $H = 1100$  kcal/kg TNT equivalent.

Scorer also found the puff radius to be  $r = \alpha \Delta h_t$ , where  $\Delta h_t$  is the cloud top height and  $\alpha$  is an empirical entrainment coefficient.  $\alpha$  ranged from 0.14 to 0.5 with a mean of 0.25. The relative dispersion  $\sigma_r = r/\sqrt{2}$ .

Using field observations, Weil<sup>14</sup> confirmed that Eq. (7) was a good fit to data over a wide range of times. Thus, Eq. (7) is suitable for the rise of a cloud before it is limited by stable stratification, e.g., an elevated inversion.

For cloud penetration of an elevated density jump, results have been found from laboratory experiments in a nonturbulent environment. Richards<sup>15</sup> obtained an empirical expression for the fraction  $P$  of the cloud penetrating the jump:  $P \simeq 1 - 0.5\Delta\rho_i/\Delta\rho_{Ti}$ , where  $\Delta\rho_i$  is the density jump and  $\Delta\rho_{Ti}$  is the average density excess of the cloud when it reaches the jump. This can be applied to atmospheric detonations and elevated temperature inversions by relating  $\Delta\rho$  to the cloud temperature excess  $\Delta\Theta$ , expressing  $\Delta\Theta$  in terms of  $F_T$  and  $r$ , and evaluating the resulting expression at  $z = h$ . From  $\Delta\rho/\rho_a = \Delta\Theta/\Theta_a$  and the above approach, one finds  $\Delta\Theta = (3/4\pi)Q_T/(\rho_a c_p r^3)$ . Richards' expression can then be rewritten as  $P = 1 - (2\pi/3)(\Delta\Theta_i \rho_a c_p \alpha^3 h^3 / Q_T)$ , where  $\Delta\Theta_i$  is the temperature jump. The  $h_s$  is assumed to be zero so that the cloud radius at  $z = h$  is  $\alpha h$ . The above relationship shows the strong sensitivity of  $P$  to  $\alpha h$ .

A more realistic temperature distribution above the CBL is a constant  $\partial\Theta_a/\partial z$ . Experiments simulating this distribution as well as a jump above a well-mixed layer are



currently underway in a salt-stratified tank at the EPA Fluid Modeling Facility in North Carolina.

**Dispersion parameters.** For clouds,  $\sigma_r$  is dominated by entrainment for short times with  $\sigma_r = \sigma_{rb} = 0.18\Delta h$ , where subscript  $b$  denotes buoyancy-induced spread. At intermediate times ( $t < T_L$ ), the  $\sigma_r$  may be dominated by ambient turbulence in the inertial subrange with  $\sigma_r \sim \sigma_{ra} = a_1 \epsilon^{1/2} t^{3/2}$ , where  $T_L$  is the Lagrangian time scale,  $\epsilon$  is the turbulent kinetic energy dissipation rate,  $a_1$  is a constant (see Thomson<sup>16</sup>), and subscript  $a$  denotes dispersion due to ambient turbulence. At long times ( $t \gg T_L$ ),  $\sigma_{ra} = (2\sigma_w^2 T_L t)^{1/2}$  for homogeneous isotropic turbulence. For  $\sigma_{ra}$ , we use an interpolation expression of the form  $\sigma_{ra} = a_1 \epsilon^{1/2} t^{3/2} / (1 + a_2 t/T_L)$  to satisfy the intermediate- and long-time results. In addition,  $\epsilon$  can be written as  $\epsilon = b\sigma_w^2/T_L$  in homogeneous isotropic turbulence.

In a strong CBL, the following approximations can be made for  $z \geq 0.1h$ :  $\epsilon \simeq 0.4w_*^3/h$ ,  $\sigma_w \simeq 0.6w_*$ , and  $T_L \sim 0.7h/w_*$  (Ref. 10). These approximations coupled with  $\epsilon = b\sigma_w^2/T_L$  lead to  $b = 0.78$ . To satisfy the long-time  $\sigma_{ra}$  limit, we must have  $a_2 = 0.62a_1$ ;  $a_1$  is estimated to be 0.57 from Thomson's two-particle model results. The resulting parameterization for  $\sigma_{ra}$  in the CBL is

$$\frac{\sigma_{ra}}{h} = \frac{0.36X^{3/2}}{1 + 0.51X} \quad \text{with} \quad X = \frac{w_* x}{Uh}, \quad (9)$$

where we have assumed  $t = x/U$  and  $X$  is a dimensionless distance or travel time.

To connect the short-, intermediate-, and long-time relative dispersion regimes in a continuous manner, we adopt the following parameterization:  $\sigma_r^3 = \sigma_{rb}^3 + \sigma_{ra}^3$ . For clouds dominated by buoyancy,  $\sigma_{rb} = 0.42F_T^{1/4} t^{1/2}$ .

The total or absolute dispersion is necessary to estimate the  $C$  for a meandering puff or plume. The  $\sigma_x$  and  $\sigma_y$  in Eq. (2) can be obtained from a parameterization of Taylor's theory:  $\sigma_x = \sigma_u t / (1 + t/2T_{Lx})^{1/2}$  and similarly for  $\sigma_y$ . The  $T_{Lx}$  is the Lagrangian time scale for the  $u$  component and can be parameterized by  $T_{Lx} \propto \sigma_u/h$ , etc. (e.g., see Ref. 6). For the CBL and the results below, we use  $T_{Lx} = T_{Ly} = 0.7h/w_*$  and  $\sigma_u = \sigma_v = 0.6w_*$ .

### Example Results

We have computed the  $C_c$  in the buoyant puff and the mean GLC along  $y = 0$  due to a meandering puff for  $0.1 \leq W \leq 50$  tons. The  $\sigma_r$ ,  $\sigma_x$ , and  $\sigma_y$  were calculated as described in the previous section. In the following, the cloud buoyancy is characterized by its dimensionless value

$$F_{T*} = \frac{F_T}{w_*^2 h^2}; \quad (10)$$

in the examples below, we use  $w_* = 2$  m/s,  $h = 1000$  m. and  $U = 5$  m/s.

Figure 1 shows calculated values of the peak ( $C_c$ )  $\text{SO}_2$  concentrations in a detonation cloud. The cloud  $\text{SO}_2$  mass is estimated from  $Q = W \cdot E_f$ , where  $E_f (= 2.23 \times 10^{-4})$ ;

Andrulis<sup>1)</sup> is the SO<sub>2</sub> emission factor. At small  $x$ , all of the curves have the same slope:  $C_c \propto x^{-3/2}$  because  $\sigma_{rb} \propto x^{1/2}$  and the  $\sigma_r$  is dominated by  $\sigma_{rb}$  near the source. For  $200 \text{ m} < x \lesssim 2000 \text{ m}$ , some curves exhibit a short region of a nearly constant  $C_c$  with  $x$ : this is due to puff trapping in the CBL and a temporary limitation on vertical dispersion due to the elevated inversion. At large distances ( $x > 10 \text{ km}$ ), clouds for all cases become uniformly mixed in the vertical but continue to spread laterally. Thus, the  $C_c$  tends towards  $Q/\sigma_{ra}^2 \propto Q/x$ ; the curves for  $W = 10 - 50$  tons show that  $C_c$  varies inversely with  $x$  for large distances.

Figure 2 shows the mean GLC  $C$  along the puff centerline ( $y = 0$ ) for the same range of  $W$  and  $F_T$  values as in Fig. 1. This mean is for an ensemble of meandering puffs and is obtained from Eq. (2) with reflection terms included. Several interesting features are found: 1) A non-monotonic variation occurs in the maximum GLC  $C_m$  with  $W$  and  $F_T$ . 2) The variation in  $C_m$  for  $0.1 \leq W \leq 50$  tons is only about a factor of 4 even though the range in  $Q$  is a factor of 500; the weak dependence on  $Q$  is attributed to the increase in  $\Delta h$  with  $F_T$ . 3) The  $C_m$  is of the order of  $0.1 \mu\text{g}/\text{m}^3$ , which is the lower bound for  $C_c$  in Fig. 1. 4) The increase in the distance to the maximum concentration with  $W$  is due to the increase in  $\Delta h$  with  $F_T$  or  $W$ .

For  $\sigma_c \gtrsim C$ , the mean GLC along  $y = 0$  due to an ensemble of meandering puffs probably has little to do with the observed centerline GLC in an individual puff. This is attributed to the large variability in individual concentration observations when  $\sigma_c \gtrsim C$ . As noted earlier, the computed  $C$  in Fig. 2 would be used together with a modeled  $\sigma_c$  in a concentration probability distribution to estimate the peak short-term GLC that could occur downstream of the detonation.

Some preliminary calculations of  $\sigma_c/C$  at the distance of the maximum GLC were made for the examples in Fig. 2. For  $W = 0.1, 1$ , and  $5$  tons, the corresponding  $\sigma_c/C$  was  $6, 2$ , and  $1.8$ ; for  $W = 10$  to  $50$  tons, the  $\sigma_c/C \lesssim 1$  and was decreasing rapidly with increasing distance. The rapid decrease was attributed to the large cloud size ( $\sigma_r$ ) relative to  $h$  and the approach of the concentration distribution to a vertically well-mixed value. The  $\sigma_c$  model requires generalization to address the  $\sigma_c$  at large distances:  $x \gtrsim (2 - 3)Uh/w_*$ , or about  $5 - 7.5 \text{ km}$  in the current example. This will be pursued in the future.

## SHORT-DURATION RELEASES

### Dispersion Model

For short-duration releases or burns, our general approach is an integrated puff model in which the short-term mean concentration relative to the puff centerline is

$$C = \int_0^{t_r} \frac{Q_r f(\mathbf{x}, t, t') dt'}{(2\pi)^{3/2} \sigma_{rx} \sigma_{ry} \sigma_{rz}} \quad (11a)$$

$$f = \exp \left[ -\frac{(x - U(t - t'))^2}{2\sigma_{rx}^2} - \frac{y^2}{2\sigma_{ry}^2} - \frac{(z - h_e)^2}{2\sigma_{rz}^2} \right], \quad (11b)$$

where  $\mathbf{x} = (x, y, z)$ ,  $t'$  is the puff emission time,  $t_r$  is the total release duration,  $Q_r$  is the continuous source emission rate,  $\sigma_{rx} = \sigma_{rx}(t - t')$ , and similarly for  $\sigma_{ry}, \sigma_{rz}$ . The integration in (11a) can be carried out analytically for limiting forms of  $\sigma_{rx}(t - t')$ , etc., but must be done numerically in general.

The integrated puff model also is used for estimating the mean concentration due to a sequence of meandering puffs by replacing the relative dispersion ( $\sigma_{rx}$ , etc in Eq. 11) by the absolute dispersion— $\sigma_x, \sigma_y, \sigma_z$ .

In the following, we calculate the  $C_c$  for a short-duration release by numerically integrating Eq. (11) with  $\sigma_{rx} = \sigma_{ry} = \sigma_{rz} = \sigma_r = a_1 \epsilon^{1/2} (t - t')^{3/2} / (1 + a_2 (t - t') / T_L)$ . Similarly, we compute the GLC  $C$  for the same release but for the meandering puffs with  $\sigma_x = \sigma_y = 0.6 w_* (t - t') / (1 + 0.5 (t - t') / T_{Lx})^{1/2}$  and  $T_{Lx} = 0.7 h / w_*$ . For an infinitely-long release, the  $C_c$  and  $C$  values should reduce to those for a continuous plume as shown below; thus the plume results serve as an upper bound to the concentration values for the short-duration release.

The mean concentration field relative to a plume centerline is given by

$$C = \frac{Q_r}{2\pi U \sigma_{ry} \sigma_{rz}} \exp \left( -\frac{y^2}{2\sigma_{ry}^2} - \frac{(z - h_e)^2}{2\sigma_{rz}^2} \right). \quad (12)$$

Here, the plume rise is attributed to buoyancy and is given by  $\Delta h = 1.6 F_b^{1/3} x^{2/3} / U$  and its radius is  $r = 0.4 \Delta h$  (Ref. 17). Source momentum effects can be included in the future. As with the puff model, we will assume  $\sigma_{ry} = \sigma_{rz} = \sigma_r$  and  $\sigma_r^3 = \sigma_{rb}^3 + \sigma_{ra}^3$ . The  $\sigma_{ra}$  is given by Eq. (11) and the plume  $\sigma_{rb} = r / \sqrt{2} = 0.45 F_b^{1/3} x^{2/3} / U$ . The  $C_c = Q_r / (2\pi U \sigma_r^2)$  from Eq. (12); these expressions are expanded to include reflection at  $z = 0, h$ .

### Example Results

Results are presented for the dimensionless concentration  $C_c U h^2 / Q_r$  for the plume and integrated-puff models, with reflection at  $z = 0, h$  included in both. The buoyancy of the continuous source is characterized by the dimensionless buoyancy flux (Ref. 10):

$$F_* = \frac{F_b}{U w_*^2 h}, \quad (13)$$

where  $F_b$  is the source buoyancy flux which is proportional to the source heat flux.

Figure 3 shows the  $C_c U h^2 / Q_r$  as a function of  $X$  for the plume model with  $F_*$  in the range  $0.001 \leq F_* \leq 0.3$ . The large variation in the dimensionless  $C_c$  at short range ( $X < 1$ ) is due to the buoyancy-induced dispersion  $\sigma_{rb}$ . As can be seen,  $C_c U h^2 / Q_r$  decreases systematically and significantly with an increase in  $F_*$  due to the increase in  $\sigma_{rb}$  with  $F_*$ . For  $X > 1$ , the curves converge to the same limit because at long times the  $\sigma_r$  is dominated by  $\sigma_{ra}$ , which is independent of  $F_*$ .

Figure 4 presents the  $C_c U h^2 / Q_r$  for both the plume and integrated-puff models for  $F_* = 0.01$  and various values of  $t_{r*} = t_r w_* / h$ , the dimensionless release duration. The time

scale  $h/w_* = 500$  s for the  $w_*$  ( $= 2$  m/s) and  $h$  ( $= 1000$  m) used here, so that  $t_r$  ranges from 50 s to 500 s or about 1 to 8 min. As can be seen, the plume result (solid curve) is an upper bound to the integrated-puff model results. The  $X$  value corresponding to the departure of the integrated-puff solution from the plume solution increases as  $t_{r*}$  does. For  $X \geq 5$ , the integrated-puff concentrations can be significantly less than the plume concentrations; this is due to the finite duration of the source.

Figure 5 shows the dimensionless mean GLC,  $CUh^2/Q_r$ , for the meandering plume and for a sequence of meandering puffs (finite-duration release). The trends with  $X$  and  $t_{r*}$  are similar to those in Fig. 4, but the near-source variation of  $CUh^2/Q_r$  with  $X$  differs from that for  $C_c$  due to the different dispersion rates in relative (Fig. 4) and absolute dispersion (Fig. 5). Note that at  $X = 0.1$ , the GLC value is about an order of magnitude smaller than the  $C_c$  (Fig. 4) because the ground is significantly removed from the elevated plume centroid. However, at  $X = 10$ , the concentration values are quite similar; this occurs because the concentration distribution becomes uniform in the vertical due to plume trapping and the horizontal spreads (relative and absolute) are about the same.

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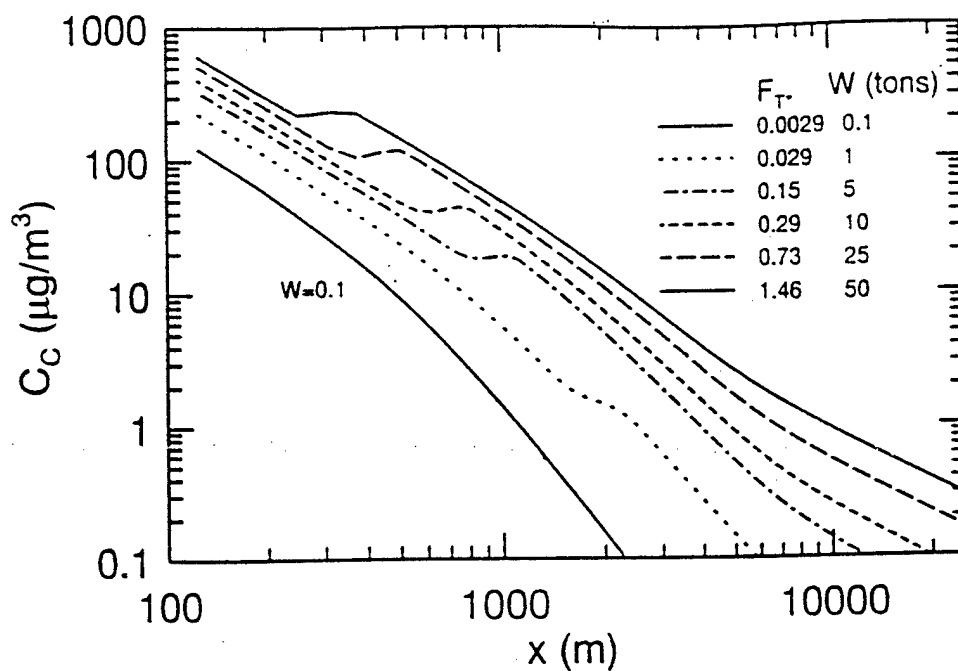


Figure 1. SO<sub>2</sub> concentration at detonation cloud centroid as a function of downwind distance and detonation mass  $W$ .

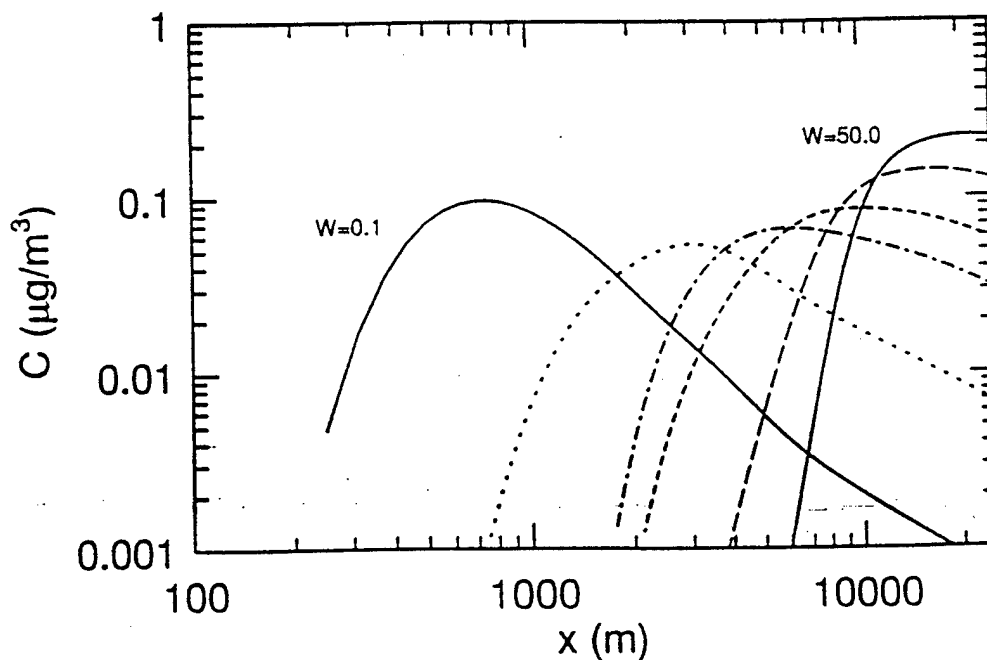


Figure 2. Mean ground-level SO<sub>2</sub> concentration along puff centerline as a function of downwind distance and detonation mass; see Fig. 1 for key to lines.

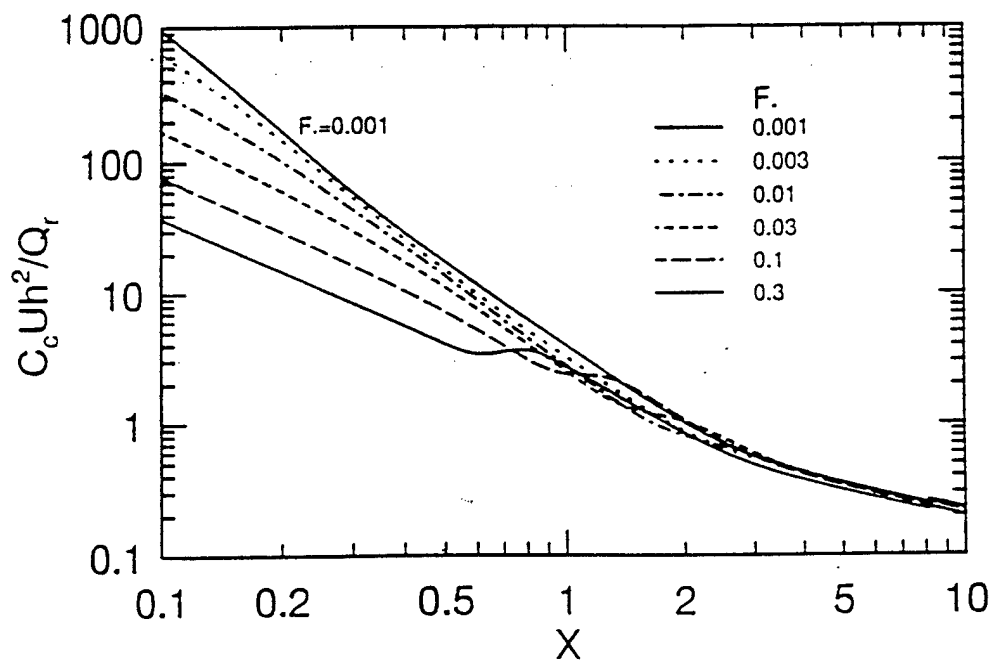


Figure 3. Dimensionless concentration at plume centroid as a function of dimensionless downwind distance and dimensionless buoyancy flux  $F_*$ .

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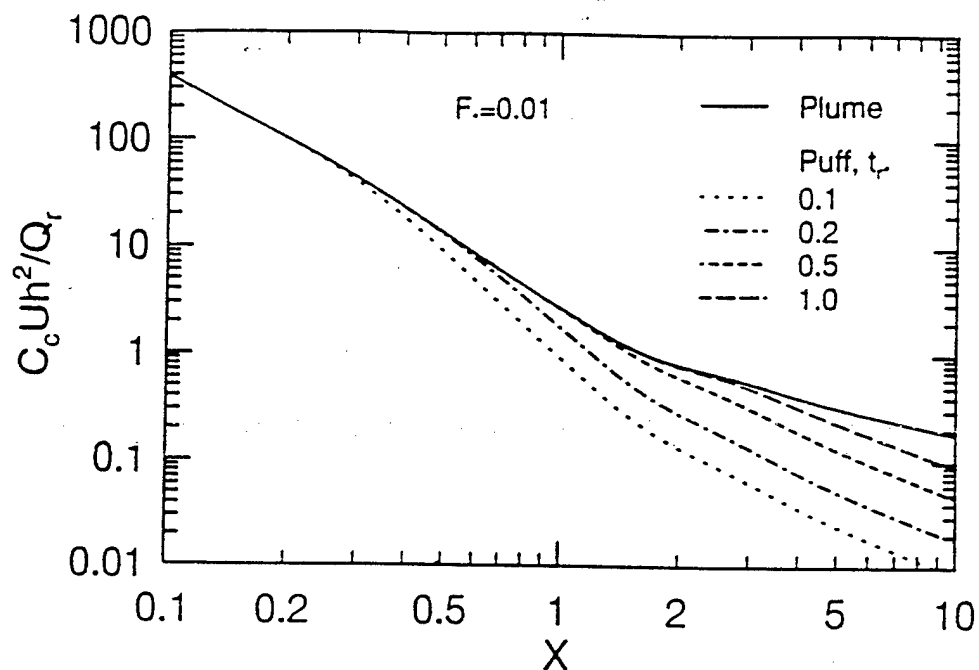


Figure 4. Dimensionless concentration at plume or puff centroid as a function of dimensionless downwind distance and dimensionless release duration  $t_{r*}$ .

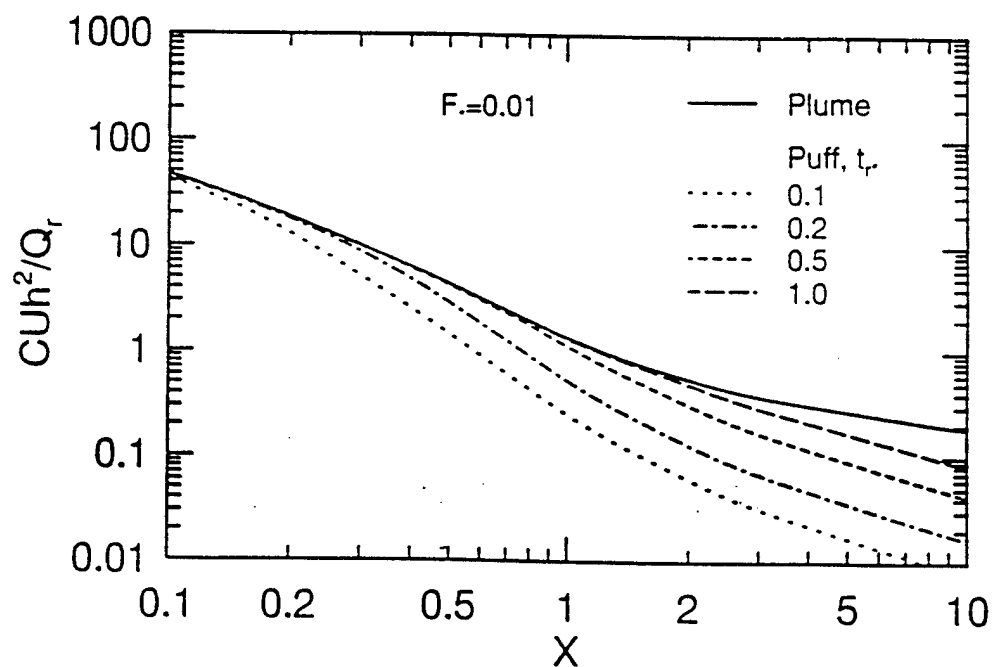


Figure 5. Dimensionless mean ground-level concentration along plume or puff centerline as a function of dimensionless downwind distance and dimensionless release duration  $t_{r*}$ .